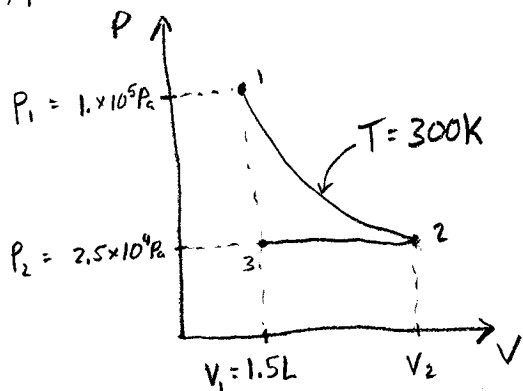


19.1



1) Since the first process is isothermal,

$pV = \text{const}$, so

$$p_1 V_1 = p_2 V_2 \Rightarrow V_2 = \frac{p_1 V_1}{p_2} = \frac{(1.0 \times 10^5 \text{ Pa})(1.5 \times 10^{-3} \text{ m}^3)}{2.5 \times 10^4 \text{ Pa}}$$

$$V_2 = 6.0 \text{ L}$$

2) The second process is isobaric, so $P_2 = P_3 = 2.5 \times 10^4 \text{ Pa}$

3) Since the pressure is constant in the second process,

$$p = \frac{nRT}{V} = \text{const.} \Rightarrow \frac{nRT_2}{V_2} = \frac{nRT_3}{V_3} \Rightarrow$$

$$T_3 = \frac{T_2 V_3}{V_2} = 300 \text{ K} \frac{1.5 \text{ L}}{6.0 \text{ L}} = 75 \text{ K}$$

4) For an isothermal process: $pV = nRT = \text{const} \Rightarrow$

$$\text{so, } W = \int_{V_1}^{V_2} p dV = nRT \int_{1.5 \text{ L}}^{6.0 \text{ L}} \frac{1}{V} dV = nRT \ln\left(\frac{6.0 \text{ L}}{1.5 \text{ L}}\right)$$

$$= p_1 V_1 \ln\left(\frac{6.0 \text{ L}}{1.5 \text{ L}}\right)$$

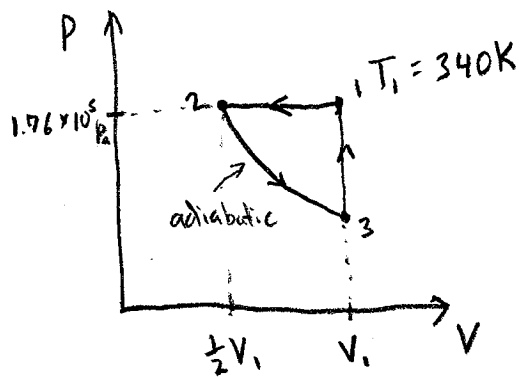
$$= (1.0 \times 10^5 \text{ Pa})(1.5 \times 10^{-3} \text{ m}^3) \ln 4$$

$$W_{1 \rightarrow 2} = 208 \text{ J}$$

5) In an isobaric process, $W = p(V_f - V_i) = (2.5 \times 10^4 \text{ Pa})(1.5 \times 10^{-3} \text{ m}^3 - 6.0 \times 10^{-3} \text{ m}^3)$

$$W_{2 \rightarrow 3} = -112.5 \text{ J}$$

19.2



1) For an isobaric process, $p = \text{const} = \frac{nRT}{V} \Rightarrow$

$$\frac{nRT_1}{V_1} = \frac{nRT_2}{V_2} = \frac{nRT_2}{\frac{1}{2}V_1} \Rightarrow$$

$$T_2 = \frac{1}{2}T_1 = 170 \text{ K}$$

2) For an adiabatic process $TV^{\gamma-1} = \text{const.} \Rightarrow$

$$T_2 V_2^{\gamma-1} = T_3 V_3^{\gamma-1}$$

now, $\gamma = \frac{C_p}{C_v} = \frac{C_v + R}{C_v}$ and since nitrogen is diatomic, $C_v = \frac{5}{2}R$

$$\therefore \gamma = \frac{\frac{5}{2}R + R}{\frac{5}{2}R} = \frac{\frac{7}{2}R}{\frac{5}{2}R} = \frac{7}{5} = 1.4$$

then $(170 \text{ K}) \left(\frac{1}{2}V_1\right)^{0.4} = T_3 V_1^{0.4}$

$$T_3 = 170 \text{ K} \left(\frac{1}{2}\right)^{0.4} = 129 \text{ K}$$

3) The minimum pressure is just the pressure at state 3, so

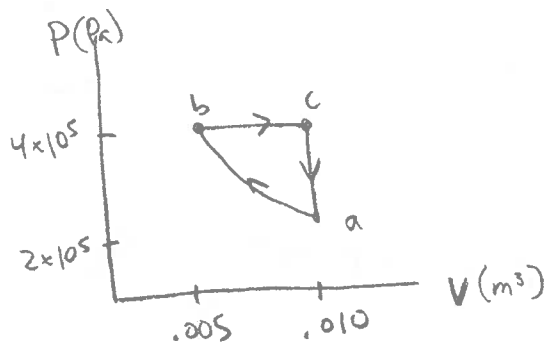
$$p_3 V_3 = nRT_3 \Rightarrow p_3 = \frac{nRT_3}{V_3}$$

$$\text{but, } V_3 = V_1 = \frac{nRT_1}{p_1} \therefore p_3 = \frac{nRT_3 p_1}{nRT_1} = \frac{(129 \text{ K})(1.76 \times 10^5 \text{ Pa})}{(340 \text{ K})}$$

$$p_3 = 6.67 \times 10^4 \text{ Pa}$$

HW #4 Solutions

20.1



(1) For isothermal process $\Phi = W = nRT \ln\left(\frac{V_b}{V_a}\right)$

since $V_b < V_a \Rightarrow W = \text{negative} \rightarrow \Phi < 0$
 $P_a V_a = 2 \times 10^5 \Rightarrow P_a V_a = P_b V_b$
 $P_b V_b = 2 \times 10^5 \quad T_a = T_b$ so heat is rejected + ab = compression

(2) bc is @ constant P $\rightarrow \Phi = n C_p \Delta T = \frac{C_p}{R} P \Delta V$

ΔV is positive so $\Phi > 0 \Rightarrow$ heat is absorbed

(3) ca is @ const. V $\rightarrow \Phi = n C_v \Delta T = \frac{C_v}{R} V \Delta P$

$\Delta P < 0$ so $\Phi < 0$ + heat is rejected

(4) $PV = nRT$

$$T_a = \frac{P_a V_a}{nR} = \frac{(2 \times 10^5)(0.010)}{(1.8)(8.314)} = 134 \text{ K}$$

$$T_b = \frac{P_b V_b}{nR} = \frac{(4 \times 10^5)(0.005)}{(1.8)(8.314)} = 134 \text{ K}$$

$$T_c = \frac{P_c V_c}{nR} = \frac{(4 \times 10^5)(0.010)}{(1.8)(8.314)} = 268 \text{ K}$$

(5) calculate Φ for each segment

$$\Phi_T = \Phi_{ab} + \Phi_{bc} + \Phi_{ca}$$

$$\Phi_{ab} = nRT \ln\left(\frac{V_b}{V_a}\right) = (1.8)(8.314)(134) \ln\left(\frac{0.005}{0.010}\right) = \underline{\underline{-1.39 \times 10^4}}$$

$$Q_{bc} = n C_p \Delta T = (1.8) \left(\frac{7}{2} \right) (8.314) (134) = 7.02 \times 10^3 \text{ J}$$

$= \frac{7}{2} R$ for diatomic

$$Q_{ca} = n C_v \Delta T = (1.8) \left(\frac{5}{2} \right) (8.314) (-134) = -5.01 \times 10^3 \text{ J}$$

$= \frac{5}{2} R$ For diatomic

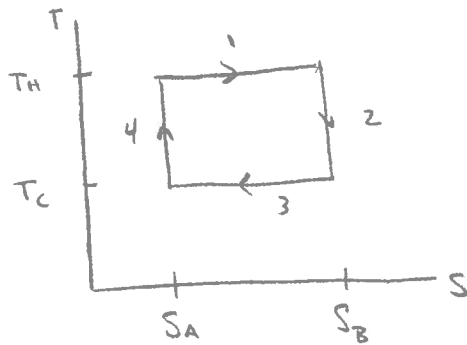
$$Q_T = (-1.39 \times 10^3) + (7.02 \times 10^3) + (-5.01 \times 10^3) = \underline{620 \text{ J}}$$

(6) For this cycle $W_{\text{net}} = Q_T = \underline{620 \text{ J}}$

(7) $e = \frac{W}{Q_H} = \frac{620 \text{ J}}{7.02 \times 10^3 \text{ J}} = 0.088 = \underline{8.7\%}$

20.2

(1) carnot cycle :



(2) For a reversible path $dS = \frac{dQ}{T} \Rightarrow dQ = TdS$

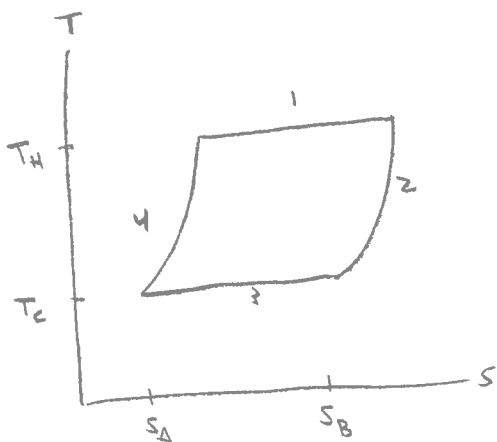
$$Q = \int dQ = \int TdS$$

for infinitesimal $dS \rightarrow dS$ and $\int TdS$ is the area under the curve in the graph above

(3) based on the graph $Q = TdS \rightarrow W = Q_H - Q_C$ ($Q_C < 0$ because $\Delta S_C < 0$)

$$e = \frac{W}{Q_H} = \frac{T_H \Delta S - T_C \Delta S}{T_H \Delta S} = \boxed{1 - \frac{T_C}{T_H}}$$

(4) Stirling cycle



$$e_{\text{stir}} = \frac{W}{Q_H} = \frac{W_{\text{stir}}}{Q_{HS}}$$

for Stirling cycle $W_{\text{stir}} = W_{\text{carnot}}$

but $Q_{HS} > Q_{HC}$ (area under curve 4+1)

because of this

$$\frac{W_{\text{car}}}{Q_{HC}} > \frac{W_{\text{car}}}{Q_{HS}}$$

$$\Rightarrow \underline{\underline{e_{\text{car}} > e_{\text{stir}}}}$$

